

Conventional Aerobic Digestion – the Basic Process

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OUTLINE

- **Process Description**
- **Regulatory Requirements**
- **Design Parameters**
- **Operational Considerations**
- **Design Example / Expected Performance**
- **Summary**

Aerobic Digestion

- **Definition:**

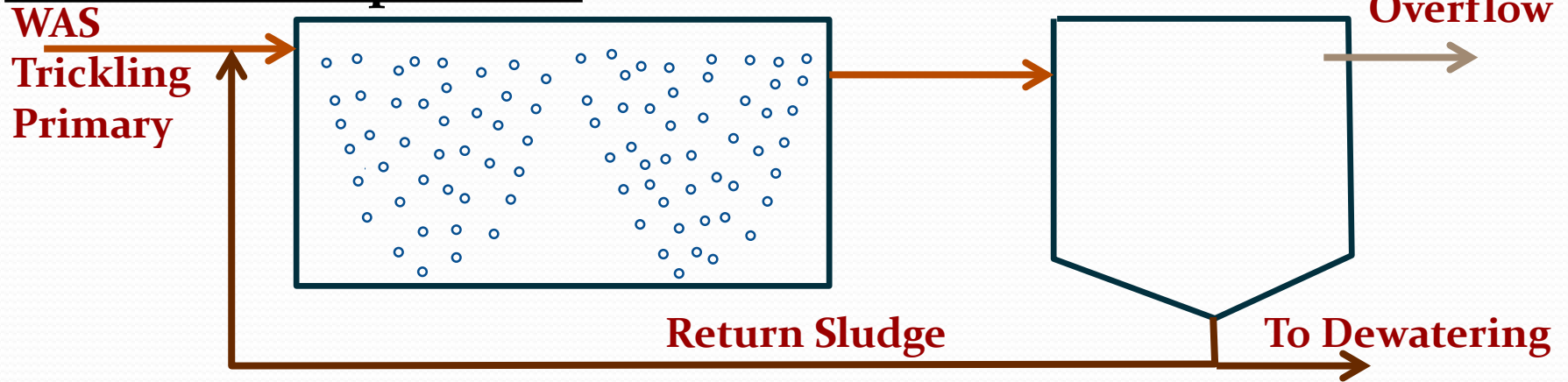
- Biological stabilization process in which aerobic reactions biologically destroy degradable organic components of biosolids removed from wastewater treatment processes

- **Objectives:**

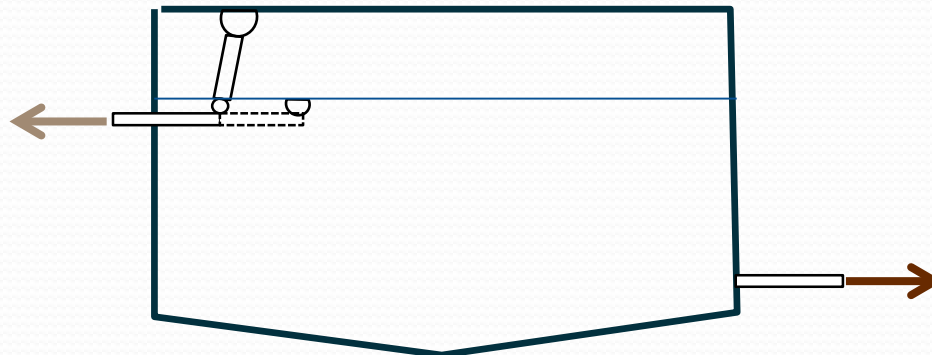
- Generation of a stable product by oxidation of biosolids organisms and other biodegradable organics
- Reduction of the biosolids mass (and volume after settling)

Configurations

Continuous Operation:



Batch Operation:



Process Theory

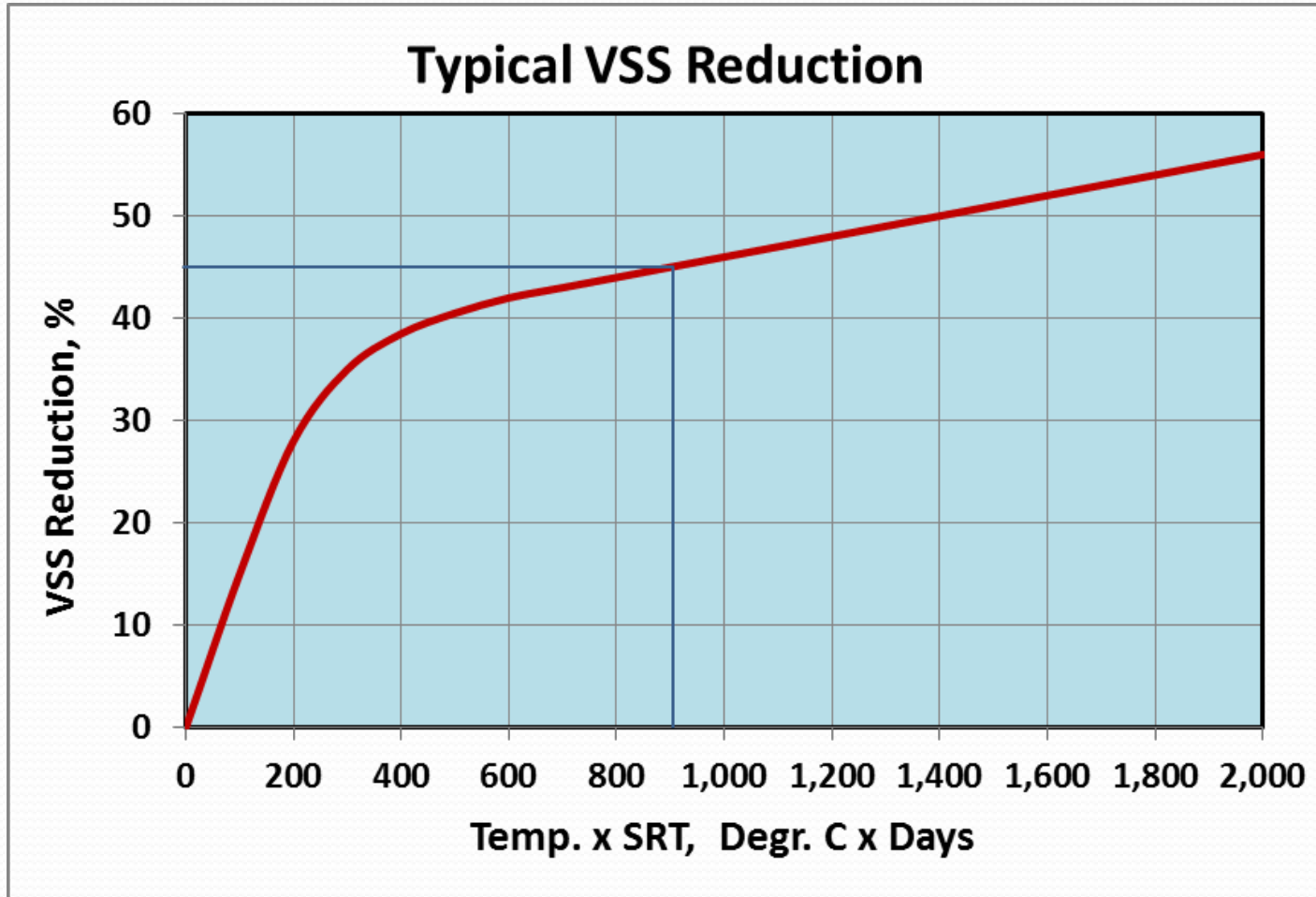
- **Aerobic biological process**
- **Similar to complete mixed activated sludge process in the endogenous phase of cell growth**
- **Energy is obtained from biodegradable organic matter, including microorganism cells**
- **Basic process chemistry:**
 - $C_5H_7NO_2 + 5O_2 \rightarrow 5CO_2 + 2H_2O + NH_3$
 - $C_5H_7NO_2 + 7O_2 \rightarrow 5CO_2 + 3H_2O + NO_3^- + H^+$
- **pH, Alkalinity drop – Lime, caustic or sodium bicarbonate might have to be added if insufficient alkalinity**

Process Theory

- **Oxygen requirements:**
 - **Carbonaceous: 1.4 lbs O₂/lb organic matter oxidized**
 - **Nitrogenous: 4.6 lbs O₂/lb NH₃-N oxidized**
 - **Total: 2 lbs O₂/lb organic matter oxidized**

Process Theory

Typical VSS Reduction (MOP-8)



Process Theory

- **Actual VSS reduction depends on:**
 - **Prior sludge processing (e.g., activated sludge type, SRT, etc.)**
 - **Sludge characteristics (e.g., portion of primary and secondary sludge, coagulant/polymer addition, volatility, etc.)**
 - **Digester operating conditions**

Regulatory Requirements

- U.S. EPA's 40 CFR Part 503 Standards for the Use or Disposal of Sewage Sludge
- Adapted by the State of Ohio under Chapter 3745-40 of the OAC

Subpart B - Land Application of Aerobically Digested Biosolids

- Pathogen reduction requirements, and
- Vector attraction reduction requirements

Regulatory Requirements

- **Class A (Exceptional Quality in Ohio)**
 - Compliance with one of seven pathogen reduction alternatives (P-8 to P-16) – **NOTE: Aerobic Digestion does not qualify**
 - Certain Fecal coliform or Salmonella densities
 - Compliance with one of eight vector attraction reduction options
 - VAR-1: 38 % reduction in volatile solids (VS) content
 - VAR-3: When the 38 % VS reduction cannot be met, additional 30-day aeration at 20 °C of digester sludge reduces VS by less than 15%
 - VAR-4: The specific oxygen uptake rate (SOUR) at 20 °C for digested sludge is less than 1.5 mg O₂ / hour / gram of dry total solids

Regulatory Requirements

- **Class B**
 - **Compliance with one of pathogen reduction alternatives P-1 to P-16**
 - **P-1: Fecal coliform density less than 2,000,000 MPN / gram of dry solids, or less than 2,000,000 cfu / gram of dry solids**
 - **P-2: Aerobic digestion – Mean CRT between 40 days at 20 °C and 60 days at 15 °C, minimum temperature always > 15 °C**
 - **Compliance with one of ten vector attraction reduction options**
 - **As for Class A (VAR-1, VAR-3 or VAR-4)**
 - **VAR-9: Subsurface injection**
 - **VAR-10: Incorporation into the soil within 6 hours of delivery**

Regulatory Requirements

- **Metal concentration limits** (for both Class A and Class B)
 - Metal ceiling concentration limits
 - Pollutant cumulative load rates

- **Ohio EPA**
 - 120 days of storage or alternative method

Design Parameters

10-State Standards

- **Aerobic sludge digestion system provisions:**
 - **Digestion,**
 - **Supernatant separation,**
 - **Sludge concentration, and**
 - **Any necessary sludge storage**
- **Multiple tanks (for avg. WWTP $Q > 0.1$ MGD)**
- **High-level emergency overflow**

Design Parameters

10-State Standards

- **Volume req'd based on Equivalent Population:**
 - 15,000 – 34,000 gal/1,000 people
 - 25% greater if solids separation in same tanks
- **Minimum air supply: 30 cfm/1,000 ft³ (D.O. = 1-2 mg/L)**
- **Minimum range of 120 to 180 days storage, unless a different period is approved by the reviewing authority**

Design Standards

- **Aeration / Mixing System:**
 - **Diffused aeration (fine and coarse bubble)**
 - **Mechanical aeration (surface, submerged turbine)**
 - **Jet aeration**
 - **Combined systems**
- **Diffused aeration is preferable in cold climates**

Operational Considerations

- **Recycle streams:** Could be high in total P and total N
- **Alkalinity depletion:** Addition of lime or caustic might be required
- **Digested sludge thickening:**
 - By gravity: 2 - 3.5%
 - Mechanically: up to 6 %
- **Digested sludge dewatering:**
 - Inconsistent
 - Better dewatering if includes primary solids
- **Foaming**
 - Foam removal, Spray, Antifoaming chemicals

Advantages and Disadvantages

- **Advantages**
 - **Low capital cost**
 - **Easy to operate**
 - **No nuisance odors**
 - **Good supernatant quality**
- **Disadvantages**
 - **Not very good dewatering characteristics**
 - **High energy cost**
 - **Significant influence by climate**

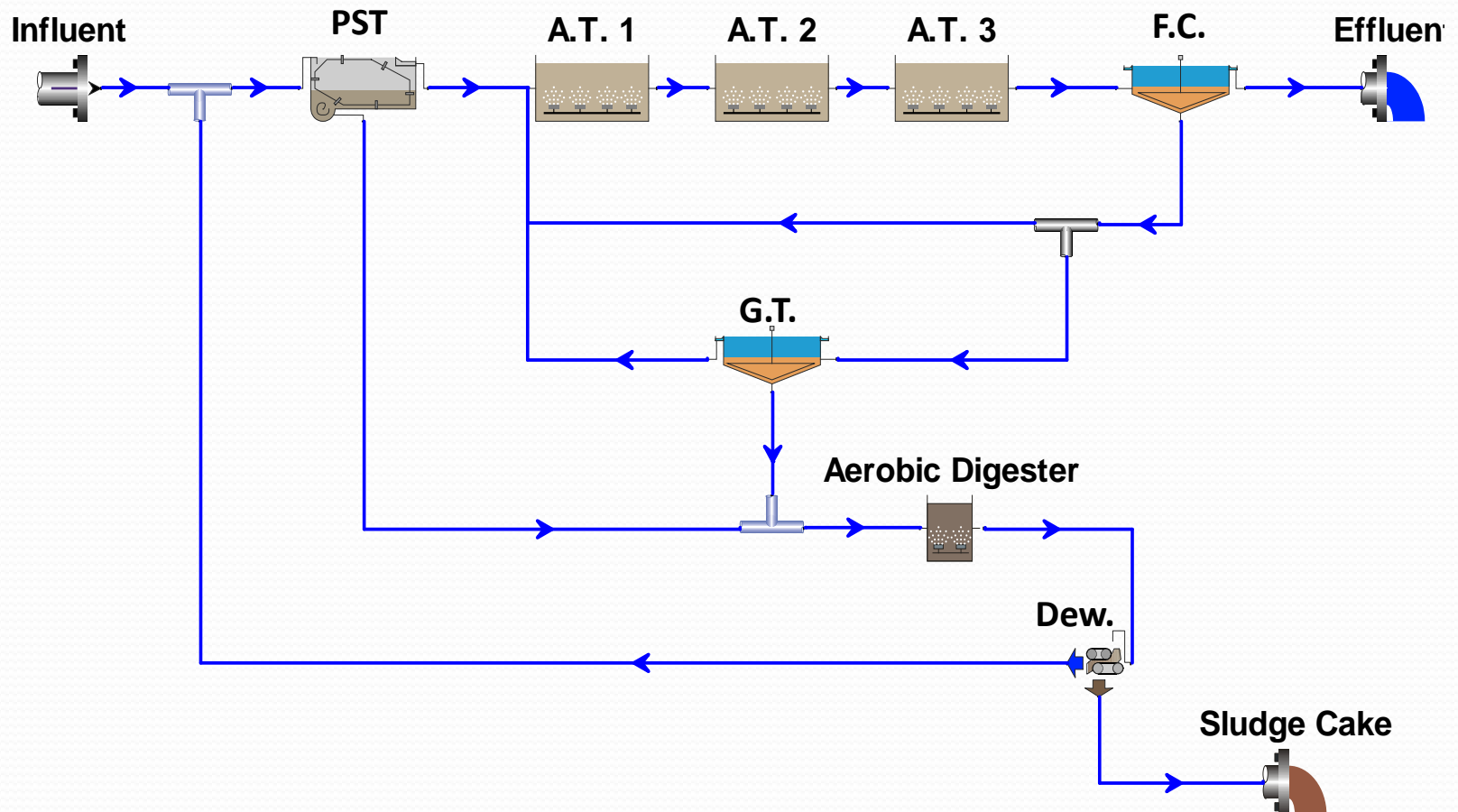
Aerobic Digester Design Example

Design Parameters:

- **Digester Influent**
 - $Q = 0.036$ MGD
 - TSS = 2%
 - VSS = 78%
- **HDT = 60 days (SRT = 60 days)**
 - $\text{Volume} = \text{HDT} \times Q = (60 \text{ days}) \times (0.0162 \text{ MGD}) = 2.16 \text{ MG}$
- **Oxygen requirements:**
 - 1 lb O₂/lb COD removed
 - 4.6 lbs O₂/lb ammonia-N removed
- **Mixing: 30 cfm/1,000 cf**

Aerobic Digestion Modeling

Using BioWin^R



Aerobic Digestion Modeling

Elements	Infl.	Prim. Infl.	Prim. Effl.	Prim. Sludge	RAS	WAS	A.D. Infl.	A.D. Effl.	Dewat. Filtrate	Sludge Cake	Final Effl.
Flow [MGD]	5	5.03	5.01	0.02	2.0	0.032	0.036	0.036	0.035	0.0015	5
TSS (mg/L)	150	152	61	22,955	8,611	8,611	20,177	11,572	362	269,391	7
VSS (mg/L)	121	121	49	18,329	6,457	6,457	15,750	7,219*	226	168,057	5
CBOD5 (mg/L)	150	149	101	12,212	2,748	2,748	9,154	574	19	13,330	3
COD (mg/L)	305	305	190	29,296	9,465	9,465	24,430	10,880	357	252,909	24
TKN (mg/L)	26	27	24	802	580	580	945	731	178	13,447	2
NH4-N (mg/L)	17	18	18	18	1	1	11	158	158	158	<1
Total P (mg/L)	5	6.4	5.1	335	322	322	472	472	203**	6,667	3.0
Alk. (mg/L)	4	4	4	4	2	2	3	0	0	0	2
pH	8	7	7	7	7	7	7	4	4	4	7
Temp. (deg. C)	15	15	15	15	15	15	15	15	15	15	15

* 54% VSS reduction

** Approximately 30% TP increase due to recycles

Aeration Requirements

Process:

- 178 lbs O₂ /Hr
- 1,160 scfm

Mixing (based on 30 cfm/1,000)

- 8,860 cfm for a 2.16-MG digester (60-day SRT/HDT)
- 4,430 cfm for a 1.08-MG digester (60-day SRT)

Aerobic Digester System

A. No Decant

- **Tanks: (Min. digester volume req'd = 2.16 MG)**
 - Four tanks 45' x 95' x 17' swd
 - Volume (each) = 0.54 MG
 - Total volume = 2.16 MG
- **Blowers: (Min. air requirements 8,860 scfm)**
 - Three 5,000-cfm each air blowers
 - Blower type: Screw positive displacement
 - Blower HP: 300 HP each
- **Diffusers: Membrane tube diffusers, 10 cfm each**
 - Number of diffusers per tank: 220

Aerobic Digester System

B. With Decant

- **Tanks: (Min. digester volume req'd = 1.08 MG)**
 - Two tanks 45' x 95' x 17' swd
Volume (each) = 0.54 MG
Total volume = 1.08 MG
- **Blowers: (Min. air requirements 4,430 scfm)**
 - Three 2,500-cfm each air blowers
 - Blower type: Screw positive displacement
 - Blower HP: 150 HP each
- **Diffusers: Membrane tube diffusers, 10 cfm each**
 - Number of diffusers per tank: 220

Summary

- **Simple and easy to operate process**
- **High energy requirements**
- **Not very effective in N.E. Ohio**
- **Requires large digestion tank volume and 120-days of storage if biosolids have to be land applied**
- **More suitable for small systems**